



# Regenerable MeO/SBA-15 nanocomposites for mid-temperature H<sub>2</sub>S removal from syngas coal gasification



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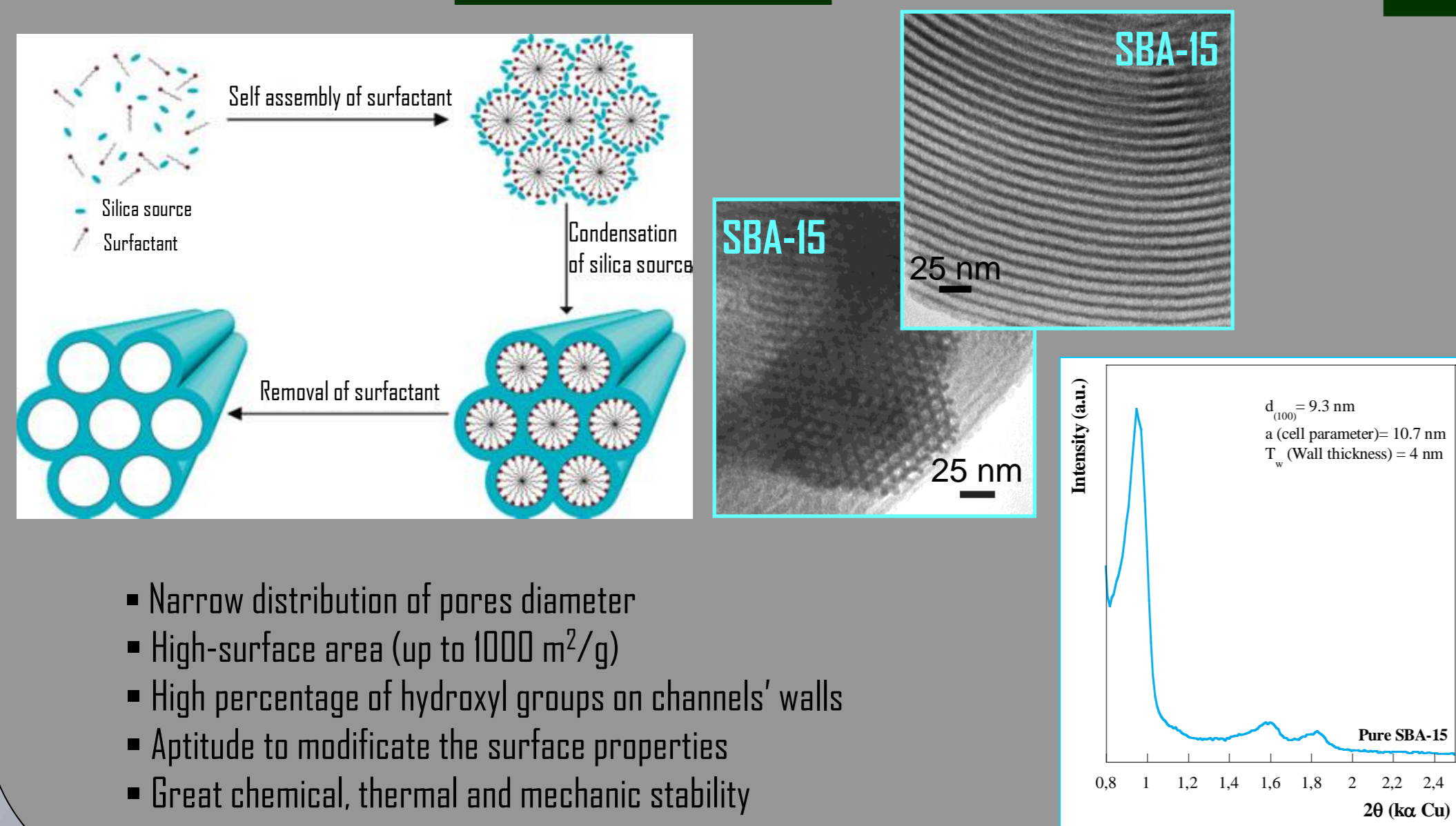
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## Introduction

These days the possible depletion of earth's fossil fuel resources and the associated environmental problems have become international concerns in the field of energy. Therefore, the development of clean and efficient coal utilization technologies is very important for the world. Raw gas produced from the IGCC gasification, the most efficient and environmentally acceptable technology, contains a lot of pollutants, including Hydrogen Sulfide (H<sub>2</sub>S), the main contaminant for air environment and for the damage to human health, water resource, catalyst poisoner and can cause pipeline corrosion thus limiting plant lifetime [1]. Zinc oxide is among the most favorable oxides to be used to remove H<sub>2</sub>S in above technologies for his high reactivity, high equilibrium constant and ability of ZnS to be regenerated. Unfortunately, despite the favourable thermodynamics, if used as pure phase, the temperatures used during the sulphurization cycle and regeneration can cause the sintering of the particles and therefore the decrease of specific surface area and, consequently, of the performance. To overcome this drawback, MeO/SBA-15 composite sorbents (Me = Zn, Fe) with good performance for mid-temperature H<sub>2</sub>S removal were synthesized in a wide range of the active phase loading.

Mesostructured SBA-15 silica is a high-surface area (up to 1000 m<sup>2</sup>/g) material, with 6-7 nm-wide regular channels and thick (3-4 nm) pore walls. By the confinement of the active phase into the mesoporous channels of SBA-15, control of the particle size on a nanometric scale might be achieved. As a consequence, enhancement of the active phase reactivity might be expected. Remarkable sulphur retention capacity referred to the active phase was shown by the composites if compared with a commercial sorbent. At variance with the case of the commercial product, the sorption properties are enhanced after regeneration and maintained upon repeating the sorption/regeneration cycle [2]. Nanocasting route has been selected to produce all the composites. The overall results show: (i) the confinement of the active phase into the ordered channel system of mesostructured SBA-15 achieved by both Incipient Wetness and Two-Solvents impregnation strategies; (ii) the sorption behaviour not strictly dependent on the surface area and pore volume features of the composites, which are usually assumed as key parameters.

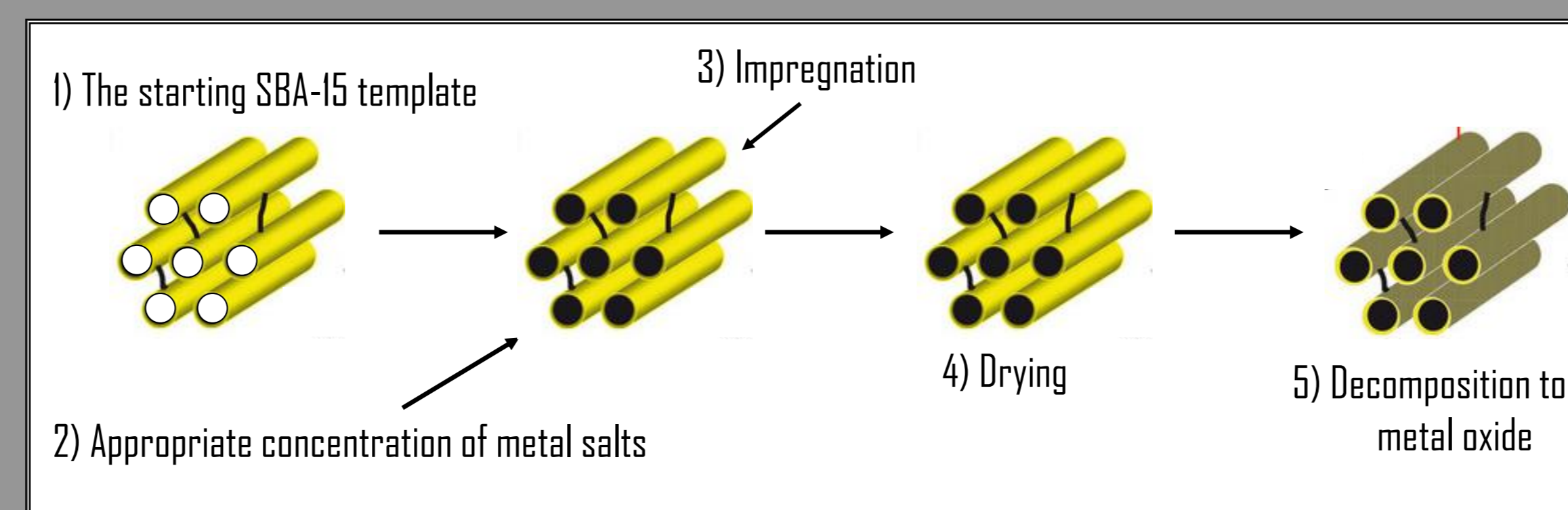
## Host Material



## Sorbents preparation: The nanocompositing method

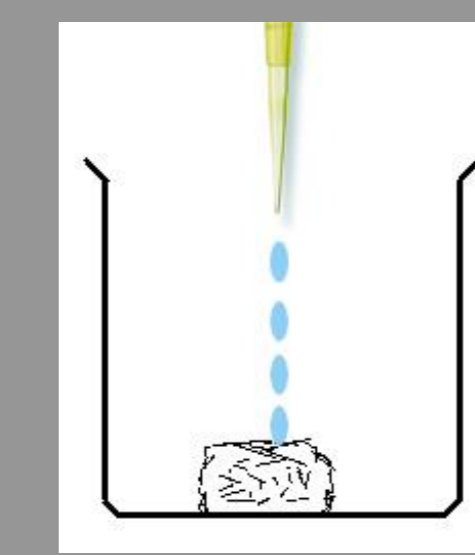
### Impregnation technique

Simplicity  
High-surface area  
High dispersion at different loadings (wt%)

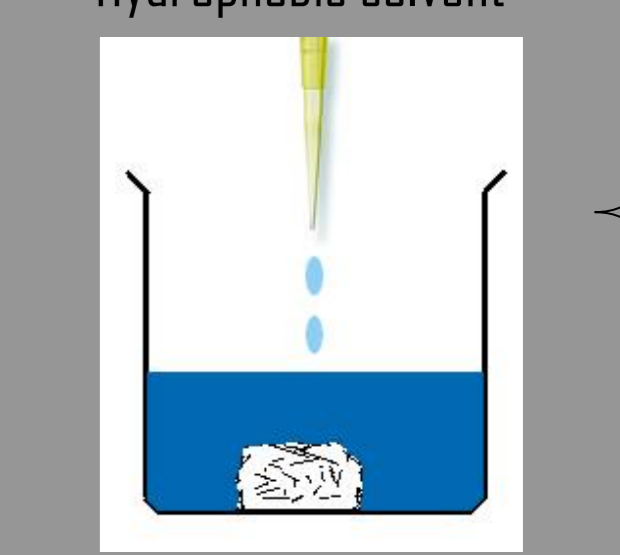


## Impregnation strategies

### Classic (one-solvent) Incipient-wetness-impregnation

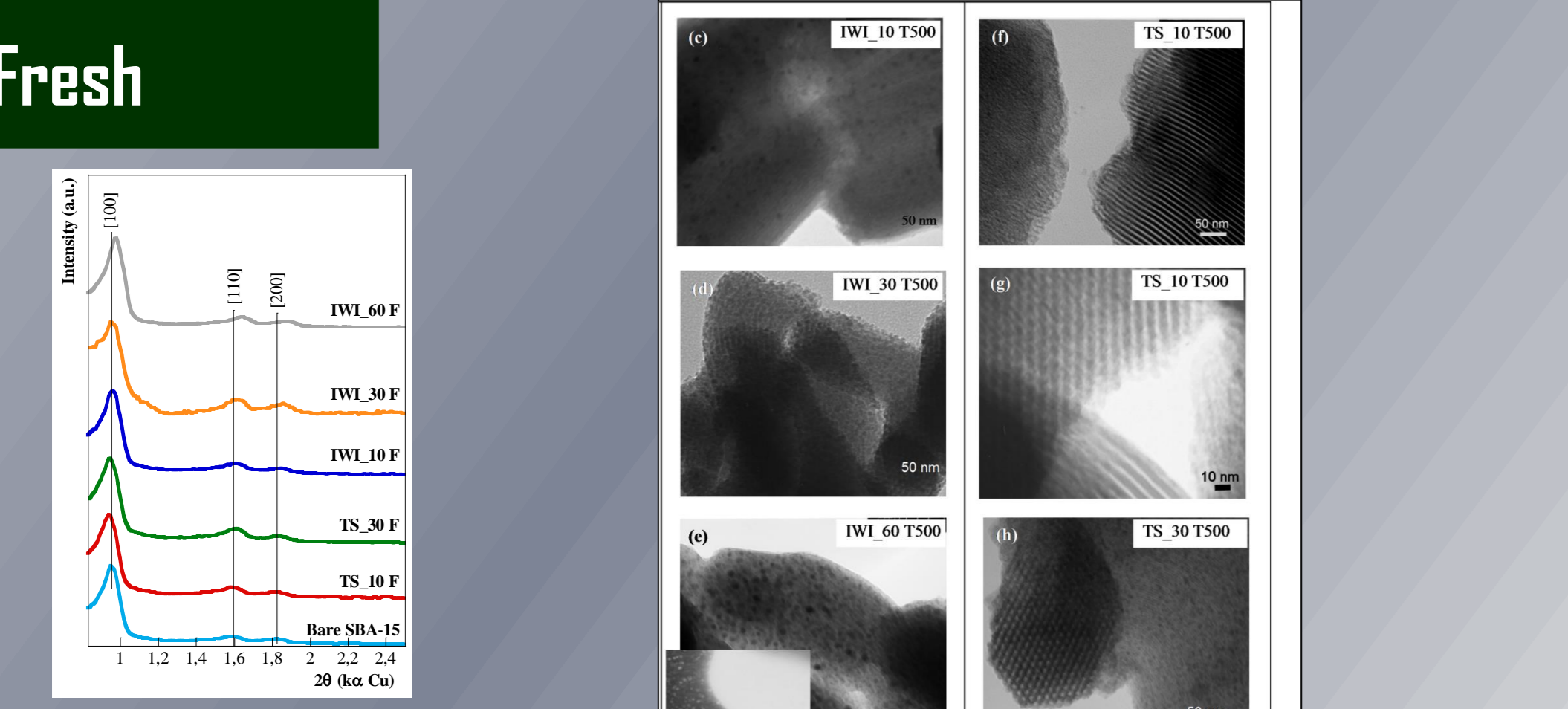


### Innovative- Two-solvents

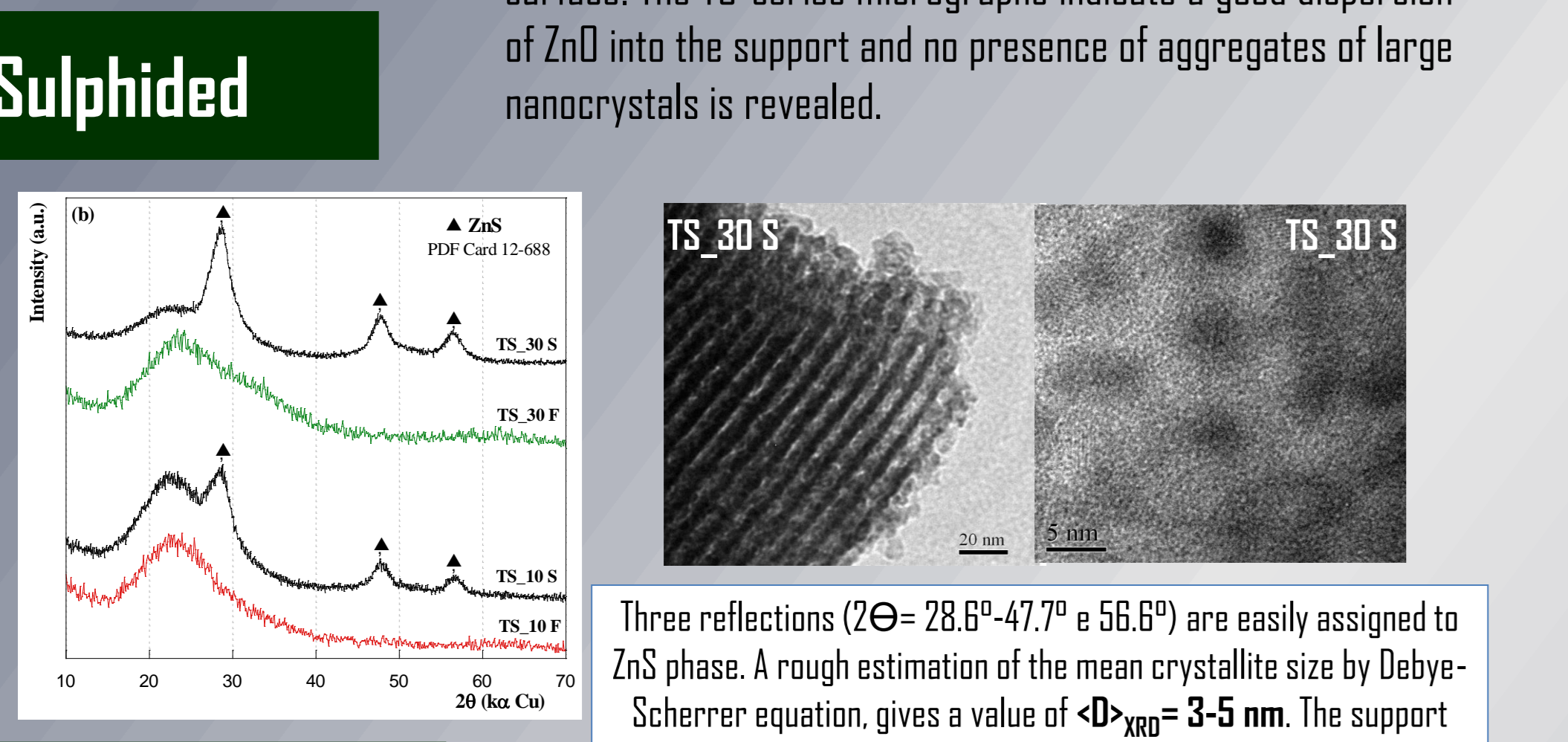


Ultrasonic bath treatment or stirring + Evacuation step + Calcination in air (minimum 500 °C)  
The Two-Solvents strategy leads to a better wettability and therefore increases the introduction of aqueous solutions into the pores, enhancing the dispersion of the metal oxide inside the pore network

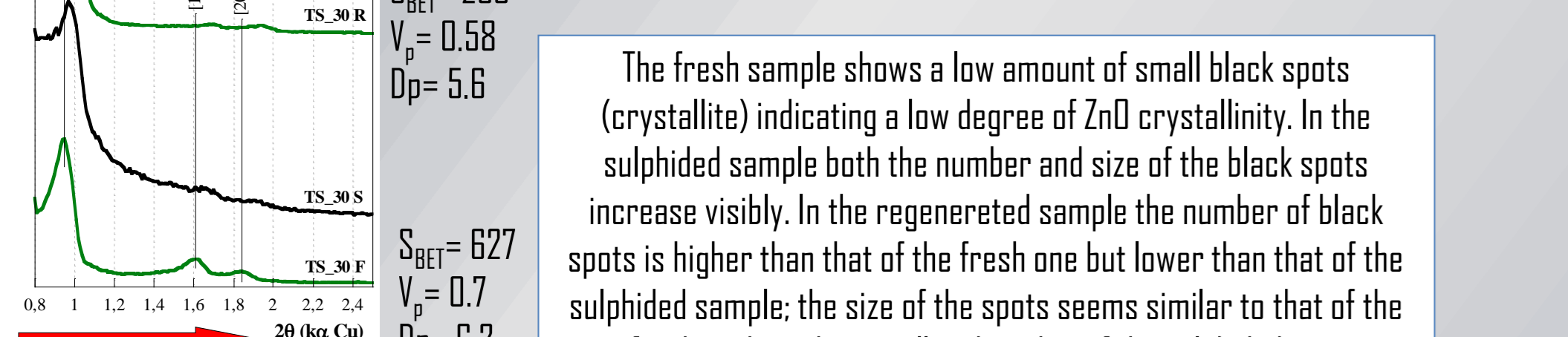
## Structural, morphological and textural features



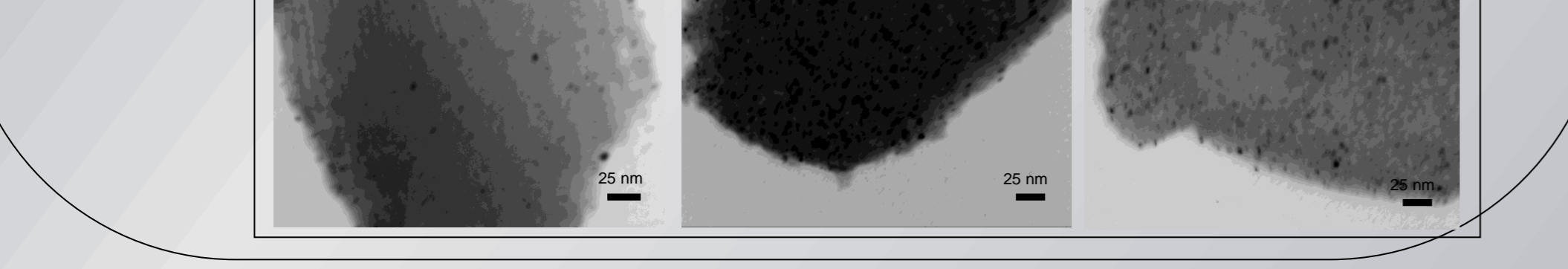
Hexagonal symmetry structure (spatial group *P6mm*) for all the composites. Shift towards higher 2θ value for IWI\_60 sample.



Three reflections (2θ = 28.6°-47.7° e 56.6°) are easily assigned to ZnS phase. A rough estimation of the mean crystallite size by Debye-Scherrer equation, gives a value of  $d_{ZnS} = 3-5$  nm. The support mesostructure is retained except for the IWI\_60 sample (not shown).



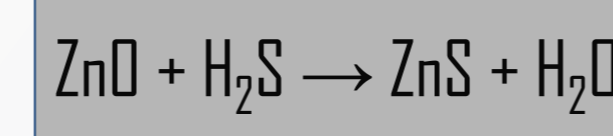
The Low-angle diffraction patterns reveals a progressive decrease shift toward higher angles: fresh > sulphidated > regenerated, which suggest a progressive decrease in the pore size.



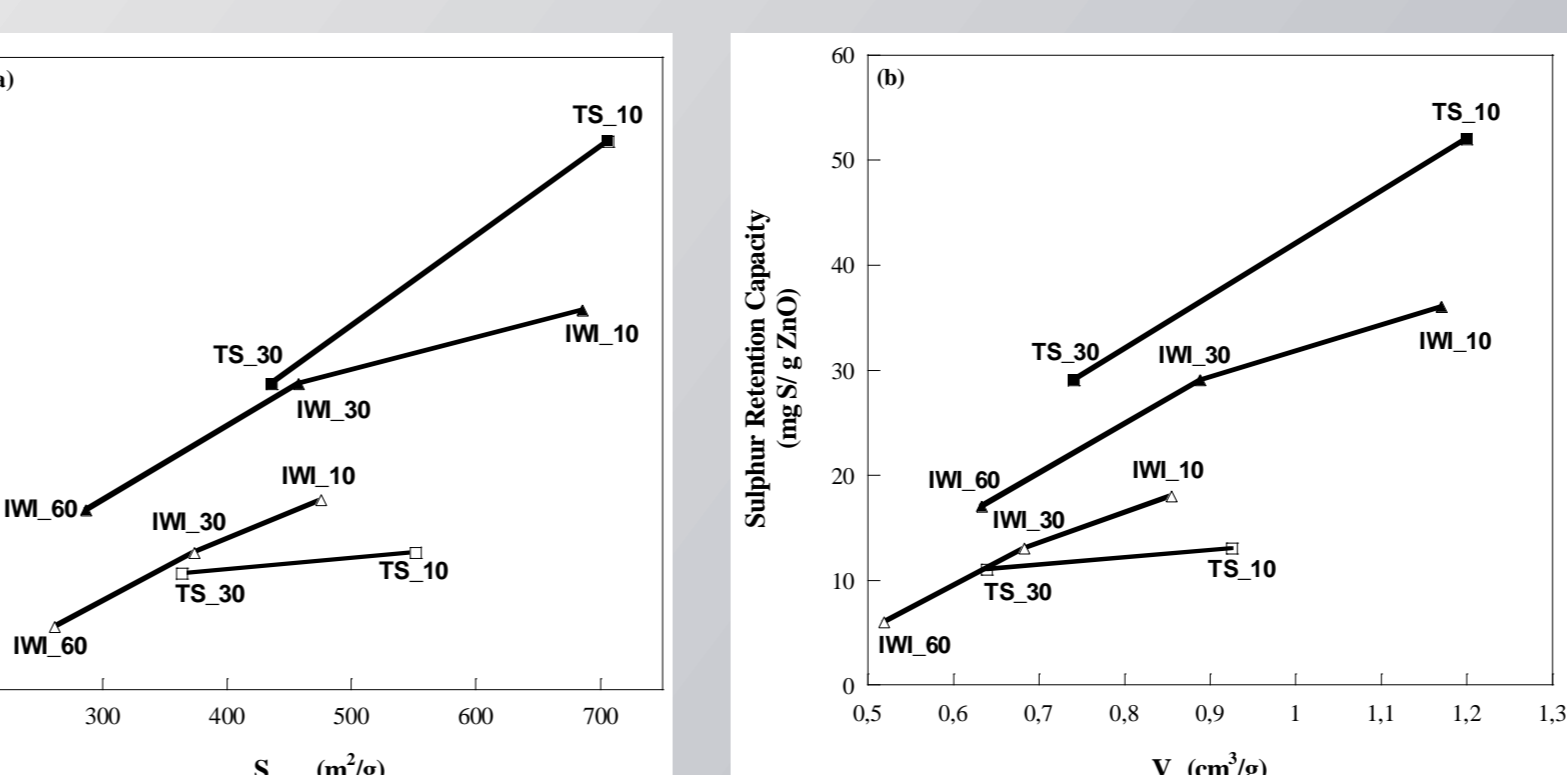
Zn<sub>2</sub>F shows only the typical halos of amorphous silica. Fe<sub>2</sub>F composite exhibits two further bands attributed to the most intense reflections of maghemite-Fe<sub>2</sub>O<sub>3</sub> phase. ZnFe<sub>2</sub>F exhibits a series of reflections ascribed to the cubic ZnFe<sub>2</sub>O<sub>4</sub> spinel nanophase

## ZnO/SBA-15 Results

### Desulphurisation test



- Quartz-made tubular reactor
- Gaseous mixture at 1.5% vol. H<sub>2</sub>S in He (0.3 mL/min H<sub>2</sub>S)
- In situ-activation with N<sub>2</sub> flow for 30 min at 300 °C (heating rate 20 °C/min)
- Mass spectrometer (MS) + thermoconductivity detector (TCD)

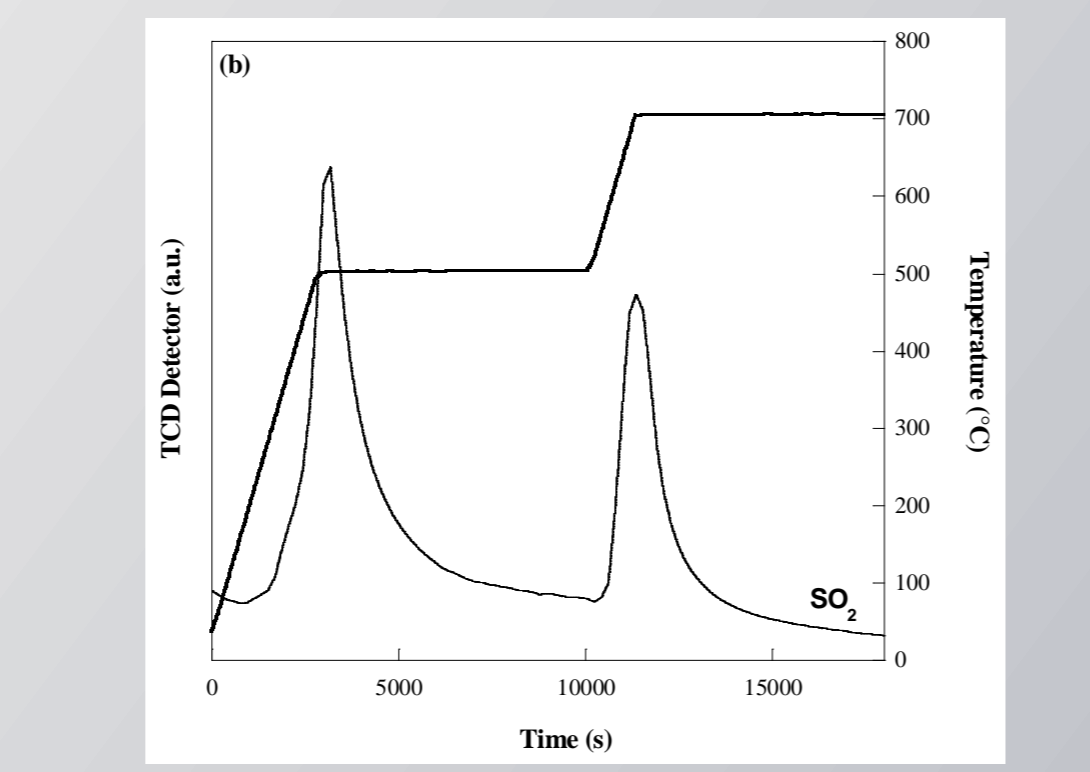
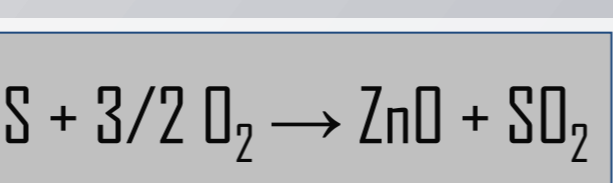


The data points cannot be interpolated by the same curve. Each set of points, as a function of preparation method (IWI or TS), requires a specific curve. The effectiveness of the active phase in the H<sub>2</sub>S removal does not depend on the textural features only. The TS-series samples lie above that of the IWI-series, which suggest that the better way of exploiting the peculiar structure of SBA-15 is the use of Two-Solvents method for the confinement of the ZnO phase into its channels.

Sample	Calcination (°C)	B <sub>t</sub> (s)	Retention Capacity (mg <sub>S</sub> /g <sub>ZnO</sub> )	Retention Capacity (mg <sub>S</sub> /g <sub>support</sub> )
Katalco <sub>30</sub> 32-5	-	100	13	13.0
SBA-15	-	-	-	-
IWI_10	500	28	36	4.0
IWI_30	600	14	18	1.8
IWI_60	500	66	29	9.0
IWI_60	600	30	13	4.0
IWI_60	500	80	17	10.0
IWI_60	600	27	6	3.6
TS_10	500	40	52	5.0
TS_10	600	10	13	1.3
TS_30	500	66	29	9.0
TS_30	600	26	11	3.4

The highest retention capacity per unit mass of ZnO is obtained for the TS\_10 sample, followed by the IWI\_10, both being much more higher than the corresponding value of the commercial ZnO sorbent. The high surface area support for dispersing on a nanometric scale the active phase enhances the ability of the latter to react with the pollutant gas.

### Regeneration test

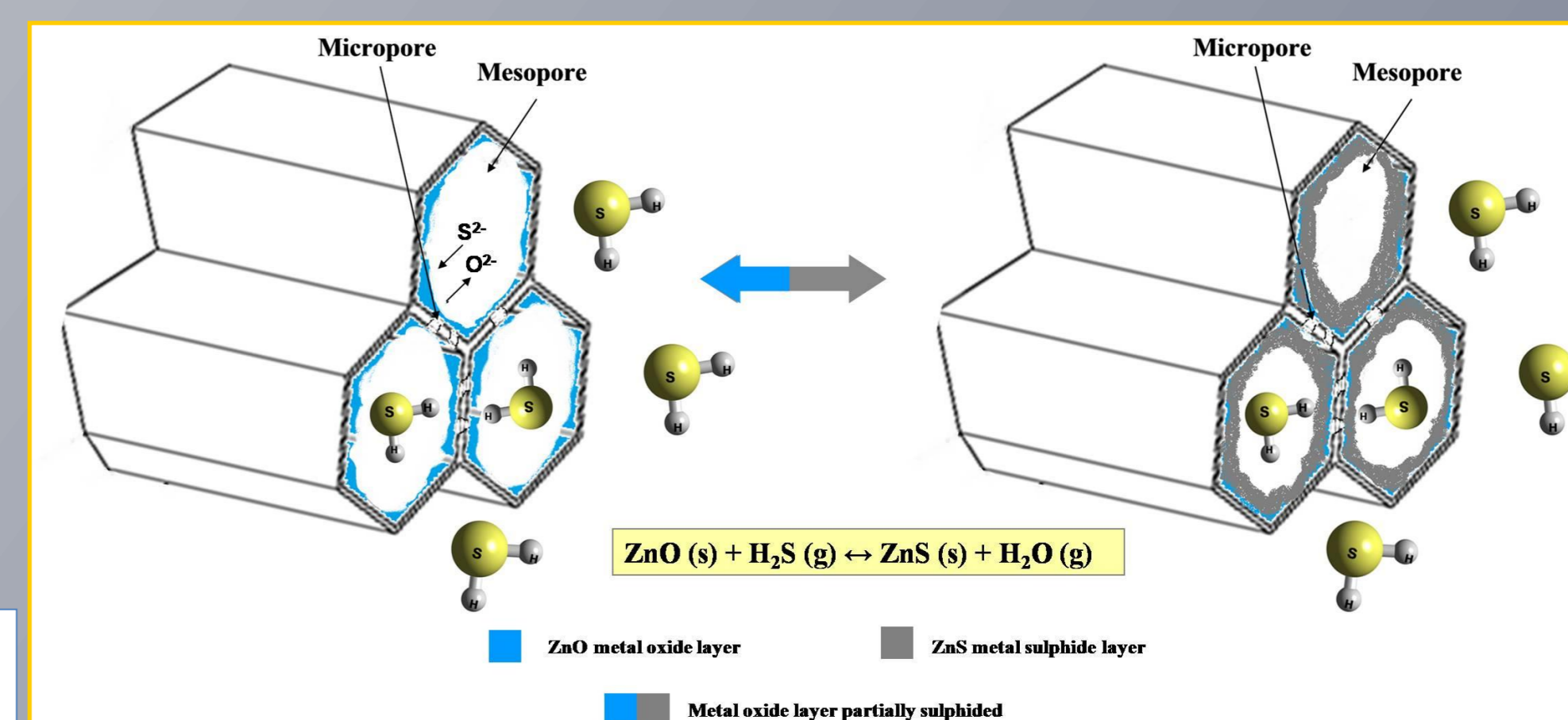


The TPD (Temperature-programmed oxidation) runs in flowing air show two peaks, corresponding to two different steps of SO<sub>2</sub> release. In view of the observed detrimental effect of the higher temperature on the sulphur retention capacity (see table above), it seems safer do not exceed 500 °C in the regeneration step.

Sample	Run number <sup>(1)</sup>	B <sub>t</sub> (s)	Retention Capacity (mg <sub>S</sub> /g <sub>ZnO</sub> )	Retention Capacity (mg <sub>S</sub> /g <sub>support</sub> )
Katalco <sub>30</sub> 32-5	1	100	13	13
	2	25	3	3
	3	25	3	3
IWI_30_T500	1	66	29	9
	2	118	51	15
	3	135	59	18
TS_30_T500	1	66	29	9
	2	92	40	12
	3	95	41	12

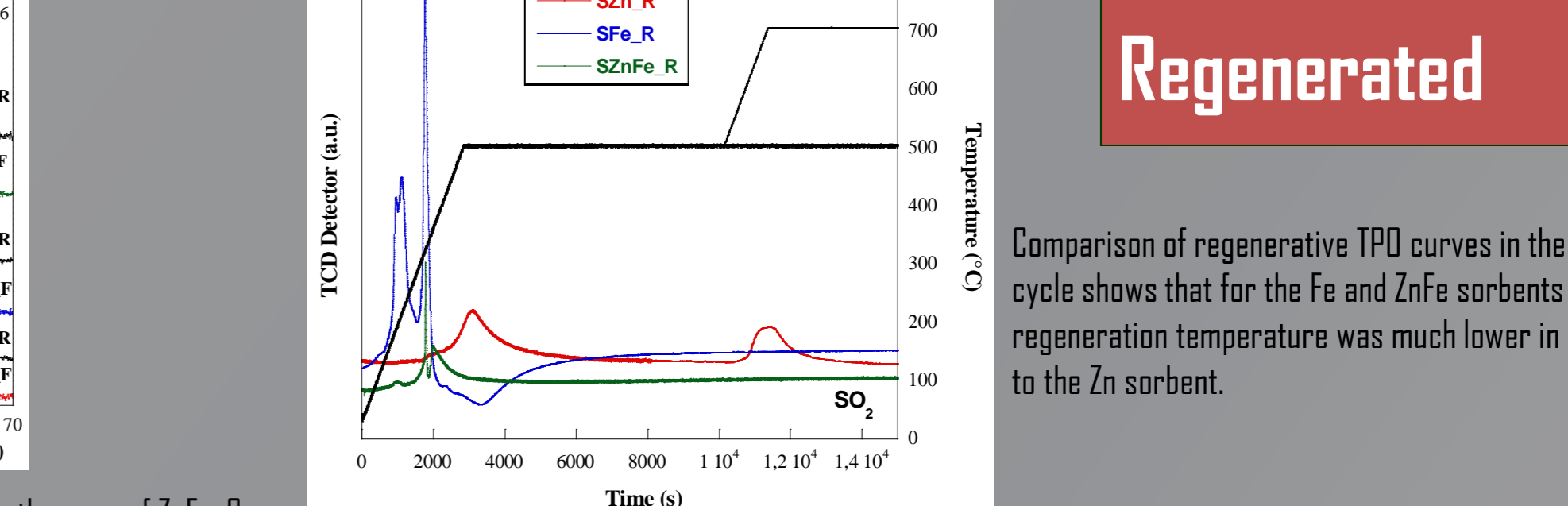
Commercial sorbent shows poor regenerative capacity. ZnO/SBA-15 composites clearly show that the regeneration process enhances their performance. Such improvement is maintaining during several cycles.

### Schematic representation of the sulphurisation process [3]



## Fe/SBA-15 and ZnFe/SBA-15 results

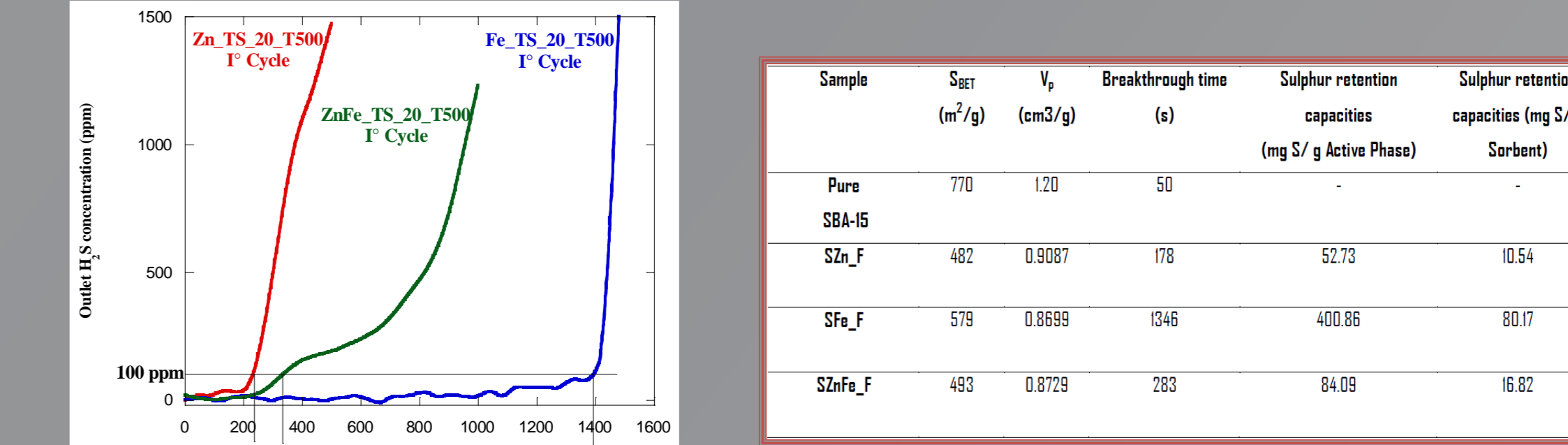
All Fe- and ZnFe-based composite sorbents were prepared via the Two-Solvents synthetic route with metal oxide loading of 20 wt. %



Comparison of regenerative TPD curves in the first cycle shows that for the Fe and ZnFe sorbents the regeneration temperature was much lower in respect to the Zn sorbent.

### Preliminary H<sub>2</sub>S sorption tests

Preliminary desulfurization breakthrough curves were obtained under the same operating conditions of sulfidation gas (20 ml/min composed of 1.5% H<sub>2</sub>S) and sorbent bed configuration (100 mg of sorbent). Remarkable differences in the breakthrough time at 100 ppm were obtained.



Sample	S <sub>02</sub> (m <sup>2</sup> /g)	V <sub>p</sub> (cm <sup>3</sup> /g)	Breakthrough time (s)	Sulphur retention capacities (mg S/g Active Phase)	Sulphur retention capacities (mg S/g Sorbent)
Pure SBA-15	770	120	50	-	-
SzZn_F	482	0.9587	178	52.73	10.54
SzFe_F	579	0.8699	1346	400.86	80.17
SzZn_F	483	0.8729	203	84.09	16.82